Introduction

This article describes the theory and calculation method for designing dilute phase pneumatic conveying systems. It is based on the work of Dr. F.A. ZENZ and Dr. D.F. OTHMER as described by them in their book "Fluidization and Fluid-Particle Systems" published in 1960 (Ref. 1). This method was later modified by Dr. Zenz based on his research work during the 70's and 80's and published in the proceedings of the Particle Science Research Institute (PSRI). Although, several other methods have been published since then, this method has been used widely and has been found to be within about 10% of the actual measured pressure drop.

This calculation method can be used to perform the following functions:

- Design of new systems.
- Prediction of maximum solids transfer rate using existing gas supply and conveying line.
- Calculations for gas flow needed for a specific solids transfer rate, using an existing conveying line.
- Sizing of the conveying line for a specific solids transfer rate using existing gas supply.
- Modifying any of the above by increasing the line diameter along the conveying line to maintain a specific conveying velocity or a terminal velocity, or a maximum conveying pressure.

1. Basis for the Calculation Method

The calculations for the design of a dilute phase conveying system are based on determining the pressure drop that is generated in the system due to the flow of gas and solids. Zenz and Othmer state that this pressure drop, for both dilute and dense phase conveying, is composed of six effective forces:

1. Friction of the gas against the pipe wall.
2. Force required for moving the solids mass through the conveying pipeline.
3. In vertical pipes the force required to support the weight of the solids.
4. In vertical pipes the force required to support the weight of the gas.
5. Force required to accelerate the solids.
6. Friction between the pipe and the solids.

Compared with dense phase, friction between the pipe and the solids (Item 6) in dilute phase conveying is usually negligible and it can be ignored.

2. Calculation Method

In their book published in 1960, Zenz and Othmer give the following two equations for calculating pressure drop in dilute phase conveying systems:

**Horizontal Lines:**

$$
\Delta R_{(H/O)} = \frac{V_g^2 \cdot \rho_g}{2 \cdot g} + \frac{W \cdot V_p}{g} + \frac{2 \cdot f \cdot \rho_g \cdot V_p^2 \cdot L}{g \cdot D} \left(1 + \frac{f_p \cdot V_p}{f \cdot V_g \cdot \rho_g} \cdot \frac{W}{V_g \cdot \rho_g} \right)
$$

**Vertical Lines:**

$$
\Delta R_{(V/ERT)} = \Delta R_{(H/O)} + \frac{W \cdot L}{L_p}
$$

For horizontal lines, the first term is the pressure drop due to the acceleration of gas, the second term is the pressure drop due to the acceleration of solids, the third term is the pressure drop due to friction between the gas and the pipe wall, and the fourth term is the pressure drop due to the flow of solids through the pipeline.

For vertical flows another term ($W \cdot L / V_p$) is added to represent the weight of the supported solids in the vertical line.

The nomenclature used in the above equations is given below:

- $V_g =$ Gas velocity
- $\rho_g =$ Gas density
- $W =$ Solids mass velocity, [lbs/sec-ft$^2$]
- $V_p =$ Particle velocity
- $f =$ Fanning friction factor
- $L =$ Length of pipeline
- $D =$ Pipeline inside diameter
- $f_p =$ Solids friction factor

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Details about the author on page 62
For pressure drop due to solids friction, Zenz and Otthmer in their book explained that some of the earlier investigations had concluded that the term \( f \cdot V^2 \) could be ignored but that the use of this term, in general, will predict pressure drops greater than those observed and thus can be considered conservative for design purposes. Further research on this topic was carried out by Zenz while he was at PSRI and he concluded that this term should be replaced by a constant \( K \) because this term was dependent upon the physical properties of the solids being conveyed. His investigation also concluded that because of many variables it was very difficult to develop an accurate correlation for calculating the value of \( K \) and therefore, the value of \( K \) should be back-calculated from the actual pressure drop data obtained from lab or plant tests.

Based on this work the term for solids pressure drop was changed to:

\[
\Delta P_s = \Delta P_{acc} + \Delta P_g + \Delta P_s + \Delta H_s + \Delta H_g + \Delta P_{misc}
\]

where,

\[
\begin{align*}
\Delta P_{misc} & = \text{Pressure drop due to miscellaneous equipment} \\
\Delta H_g & = \text{Pressure drop due to elevation of gas by } \Delta Z \text{ feet} \\
\Delta H_s & = \text{Pressure drop due to elevation of solids by } \Delta Z \text{ feet} \\
\end{align*}
\]

The next step is to develop a single equation for calculating the total pressure drop in a conveying system that may have both horizontal and vertical lines. In addition, a term \( \Delta P_{misc} \) was added to account for pressure drop in any equipment such as a dust collector that may be required at the end of the conveying line.

This equation consisting of six pressure drop terms is given below:

\[
\Delta P_{total} = \Delta P_{acc} + \Delta P_g + \Delta P_s + \Delta H_s + \Delta H_g + \Delta P_{misc}
\]

where,

\[
\begin{align*}
\Delta P_{total} & = \text{total pressure drop in the system} \\
\Delta P_{acc} & = \text{Pressure drop due to acceleration of the solids from their "at rest" condition at the pick-up point to their conveying velocity up to the exit from the conveying system} \\
\Delta P_g & = \text{Pressure drop of gas due to frictional losses between the gas and the pipe wall} \\
\Delta P_s & = \text{Pressure drop of solids through the pipeline} \\
\Delta H_g & = \text{Pressure drop due to elevation of gas in vertical pipe} \\
\Delta H_s & = \text{Pressure drop due to elevation of solids in vertical pipe} \\
\Delta P_{misc} & = \text{Pressure drop due to miscellaneous equipment}
\end{align*}
\]

These six pressure drop terms given above are related to the two pressure drop equations given by Zenz and Otthmer. These terms are then converted to the units that are commonly used in pneumatic conveying systems, resulting in the following equations where pressure drop is expressed in lbs/square inch.

Eq. 1: Pressure drop due to acceleration of the solids from their "at rest" condition at the pick-up point to the conveying velocity up to the exit from the conveying system:

\[
\Delta P_{acc} = \frac{W \cdot V_s}{144 \cdot g} - \frac{W \cdot V_p}{4640}
\]

Eq. 2: Pressure drop of gas due to frictional losses between gas and the conveying pipeline and in any bends, diverter valves, and flexible hoses that may be in the pipeline:

\[
\Delta P_g = \frac{4f \cdot L \cdot \rho_g \cdot V^2}{2g \cdot D \cdot 144}
\]

Note: In the above expression, the term "L" is the length of the straight sections of the pipeline and is the "equivalent length" of the bends, diverter valves and flexible hoses.

Eq. 3: Pressure drop due to friction between the solids and the conveying pipeline, bends, diverter valves, and flexible hoses:

\[
\Delta P_s = \Delta P_{acc} \cdot K \cdot R \quad \text{(modified Zenz equation)}
\]

Eq. 4: Pressure drop due to elevation of gas by \( \Delta Z \) feet:

\[
\Delta H_g = \frac{\Delta Z \cdot \rho_g}{144 \cdot \frac{V_p}{g}}
\]

Eq. 5: Pressure drop due to elevation of solids by \( \Delta Z \) feet:

\[
\Delta H_s = \frac{\Delta Z \cdot W}{144 \cdot \frac{V_p}{g}}
\]

Eq. 6: Pressure drop due to miscellaneous equipment in the conveying system:

\[
\Delta P_{misc} \quad \text{(ft is a term that is not calculated but is entered as input data in the calculations). This term is a constant.}
\]

Nomenclature

The nomenclature and the units that are used in the above six equations are given below:

\[
\begin{align*}
D & = \text{Pipe inside diameter (ft)} \\
f & = \text{Fanning friction factor} \\
g & = \text{Acceleration due to gravity (32.2 ft/sec}^2) \\
g_c & = \text{Constant (32.174 ft-lb/ft-sec}^2) \\
K & = \text{Friction multiplier for the solids conveyed} \\
L & = \text{Pipe equivalent length (ft)} \\
R & = \text{Solids to gas mass flow ratio (lb/ft)} \\
V_g & = \text{Gas velocity (ft/sec)} \\
V_p & = \text{Particle velocity (ft/sec)} \\
W & = \text{Solids line loading (lbs/sec-ft)} \\
Z & = \text{Elevation change in conveying line (ft)} \\
\rho_g & = \text{Gas density (lbs/ft}^3) \\
\end{align*}
\]

To solve the above equations the value of the following terms has to be determined:

\[
\begin{align*}
f & = \text{Fanning friction factor} \\
K & = \text{Friction multiplier} \\
L & = \text{Pipe equivalent length} \\
V_p & = \text{Solids velocity} \\
R & = \text{Solids to Gas ratio} \\
\end{align*}
\]

These values are determined as follows:
2.1 Fanning Friction Factor \( f \)

The Reynolds number \( (N_{Re}) \) is first calculated

\[ N_{Re} = \frac{D \cdot V_g \cdot \rho_g}{\mu_g} \]

where \( \mu_g \) is the gas viscosity in lbs/(ft·sec)

After this, the Fanning friction factor is calculated using the following equation developed from the charts given in CRANE’s Technical Paper No. 410 (pages A-23, A24) on the “Flow of Fluids”.

Eq. 7:

\[ f = \frac{0.331}{\log_{10}\left[\frac{\varepsilon}{3.7 \cdot D} + \left(\frac{f}{N_{Re}}\right)^{0.75}\right]} \]

where \( \varepsilon \) is the pipe roughness factor. Pipe roughness factor depends on if the pipe is internally smooth, rough, or very rough. The value of this factor based on test data is given below:

- for internally smooth pipes, \( \varepsilon = 0.00015 \);
- for shot-peened pipes, \( \varepsilon = 0.0005 \);

2.2 Friction Multiplier \( (K) \)

The value of the Friction Multiplier \( (K) \) is not calculated but is determined experimentally or retrieved from data bank. Its value is different for different materials. Its range is typically 0.4 to 4.0

2.3 Pipe Equivalent Length \( (L) \)

For straight pipes use the actual length of the pipe.

For components such as bends, diverter valves, and flexible hoses, use their equivalent length expressed in pipe diameters of the conveying pipe. Typical equivalent length values are given below:

<table>
<thead>
<tr>
<th>Component:</th>
<th>Equivalent Length</th>
</tr>
</thead>
<tbody>
<tr>
<td>Bends</td>
<td></td>
</tr>
<tr>
<td>90° bend, long radius, (10 to 1 radius to diameter ratio):</td>
<td>40, or 20 ft whichever is more</td>
</tr>
<tr>
<td>Diverter Valves</td>
<td></td>
</tr>
<tr>
<td>45 degree divert angle:</td>
<td>20</td>
</tr>
<tr>
<td>30 degree divert angle:</td>
<td>10</td>
</tr>
<tr>
<td>Flexible Hoses</td>
<td></td>
</tr>
<tr>
<td>Stainless steel, with lined interior:</td>
<td>3 x pipe length</td>
</tr>
<tr>
<td>Rubber or vinyl hose:</td>
<td>5 x pipe length</td>
</tr>
<tr>
<td>For bends that are less than 90°, use equivalent length as:</td>
<td>( = 40 \cdot \frac{\text{Degree of Bend}}{90} )</td>
</tr>
</tbody>
</table>

For special bends such as short radius bends, Hammertec, Gamma, pocket-T’s, etc., increase the value of 40 to a higher number. For example, for a typical conveying system with about 5 bends increase the calculated pressure drop value by 10%. For 10 bends increase it by 20%. These numbers are based on lab tests or plant data.

2.4 Solids Velocity \( (V_p) \)

Solids velocity is always less than the gas velocity because of the drag forces between the gas and the solids. This difference is called the slip factor. For most of coarse or hard solids this slip factor is about 0.8, which means that the solids velocity is 80% of the gas velocity. Therefore, for these materials use a solids velocity 20% less than the gas velocity \( V_g \), i.e. \( V_p = 0.8 \cdot V_g \)

For fine powders solids velocity is closer to the gas velocity. For these materials use a slip factor of 0.9 instead of 0.8. This value generally ranges from 0.7 to 0.95. Lighter and smaller materials have higher values than those of larger and heavier particles.

2.4.1 Solids Velocity in Long Radius Bends

For a 90 degree radius bend, solids velocity at the exit of the bend \( V_{p2} \) is 0.8 times the solids velocity at the inlet of the bend \( V_{p1} \). The factor “0.8” is a typical value but it ranges from 0.6 to 0.9 depending upon the properties of the solids. For bends that are less than 90 degrees, the exit velocity \( V_{p2} \) is

\[ V_{p2} = \left[ 1 - \frac{\text{Degree of bend}}{90} \right] \cdot (1 - 0.8) \cdot V_{p1} \]

2.4.2 Solids Velocity after Leaving a Bend

After leaving a 90 degree bend, use a default value of 20 pipe diameters to calculate the length of the straight pipe for the solids to re-accelerate to their original velocity at the inlet of the bend \( (V_{p1}) \).

2.5 Solids to Air Ratio \( R \)

Calculations are based on using the following term as given by ZENZ and OTHMER:

\[ R = \frac{W}{V_p \cdot p_g} = \frac{m}{A \cdot V_p \cdot p_g} \]

Where \( m \) is the solids mass flow rate in lbs/sec and \( A \) is the cross-sectional area of the pipe in ft². The gas mass flow rate in lbs/sec is calculated based on the actual cfm of gas and gas density introduced into the conveying system by the gas mover, and the internal cross-sectional area of the pipe. Gas can be air or any other gas. Use air as default if use of a different gas is not given.

For pressure type conveying systems, reduce the gas mass flow rate by 5% (default value) to account for gas leakage through a rotary valve, if a rotary valve is used to feed the solids. For more accurate results, change this default value by calculating actual rotary valve leakage (both clearance and displacement).

For the gas density term \( p_g \), make corrections if the inlet conditions are different from standard conditions (68 °F, 14.7 psia).

2.6 Gas Density along the Conveying Line:

Gas density depends upon gas pressure and temperature. For most conveying systems, gas temperature can be assumed to be constant. Therefore, only changes in pressure will change the gas density. Because the pressure either increases or decreases along the conveying line, depending upon whether it is a vacuum system or a pressure system, gas density will also keep on increasing or decreasing. For calculating the pressure drop due the flow of gas, divide the conveying line into small lengths such as 5 or 10 ft, start from the point where inlet gas density is known (such as ambient conditions), and calculate the exit pressure and corresponding gas density for this small
section. Then use this exit gas density as the inlet gas density for the next pipe section. Repeat this procedure until reaching the end of the conveying line. For vacuum systems, start from the pick-up point and end at the blower inlet. For pressure systems, start from the end of the conveying line and return to the pick-up point.

2.7 Addition or Removal of Gas along the Conveying Line

If some conveying systems, gas is added or removed from the conveying system at any point along the route of the conveying line. In this case, re-calculate the gas mass flow and the solids to gas ratio, and use the new gas flow for the pressure drop calculations after this injection point.

3. Calculation Procedure

The procedure given below for running these calculations is based on the Microsoft Excel spreadsheet method.

3.1 Step 1:

The first step is to define the objectives for the calculations and to gather data that is needed for these calculations.

Example: Conveying System Objectives and Design Data:

Let us assume that the main objective for the calculations is to determine the pressure drop in a vacuum type dilute phase pneumatic conveying system conveying polyethylene pellets at 10,000 lbs/hr rate through a proposed conveying line. Assume that the line diameter is 4 inch but that it can be changed if the calculated pressure drop does not fall within the vacuum rating of the conveying blower. Conveying system uses ambient air at standard conditions. Starting from the inlet, the conveying line is 80 feet horizontal, then has a 90 degree long radius bend, then a 40 feet vertical section, then a 90 degree long radius bend, then a 40 feet horizontal section, then a 90 degree horizontal bend, and lastly 10 feet of horizontal pipe. Pipeline is internally scored to prevent streamers. Conveying line material is aluminum. Ambient conditions are 14.7 psia and 72 F. Air density at these conditions is 0.075 lbs/cu ft. Pick-up velocity is 65 ft/sec. Solids velocity is 80% of gas velocity. Solids friction factor is 1.2. Pipeline roughness factor is 0.0005.

3.2 Step 2:

From the equations given above, retrieve the formulae that will be required in the calculations. These formulae are given below:

Formulae used in Calculations:

| Flow of Solids: | $\Delta P_g \cdot K \cdot R$ |
| Elevation of gas: | $\frac{\Delta Z \cdot \rho_g \cdot g}{144 \cdot g_c}$ |
| Elevation of solids: | $\frac{\Delta Z \cdot W \cdot g}{144 \cdot V_f \cdot g_c}$ |
| Misc. Pressure Drop: | Assume that it is in a dust collector at the end of the conveying line and is 0.2 psi. |

3.3 Step 3:

Enter the input data in a spreadsheet form as shown in worksheets 1 and 2. Enter all of the input data in worksheet 1 except for the conveying pipeline data. Enter the pipeline data as shown in worksheet 2 starting from the beginning of the pipeline and finishing at its end.

Prepare worksheet 3 for running the pressure drop calculations. In this sheet, before starting the calculations, all of the cells will be empty except for the known inlet conditions: gas temperature, inlet gas density, inlet pressure, and inlet gas (pick-up) velocity. Pipeline sections are numbered the same as in worksheet 2.

3.4 Step 4: Calculations

3.4.1 Pressure Drop Calculations

In worksheet 1, calculate the Fanning Friction Factor by entering its formula in the formula bar. Use this friction factor in calculating the pressure drop due to the flow of the gas in worksheet 3. Keep this factor constant in the gas pressure drop calculations for all of the pipe sections. Now start the pressure drop calculations in worksheet 3 starting from the first pipe section. Enter the formula for the pressure drop due to the flow of gas, $(4 \cdot f \cdot L \cdot \rho_g \cdot V_f^2)/(9266 \cdot D)$, in cell B2 using cell numbers for the input data. For example, the cell numbers will be as follows:

- For $f$ worksheet 1, B16
- For $L$ worksheet 2, F2
- For $\rho_g$, worksheet 3, J2
- For $V_f$, worksheet 3, N2

For $D$, worksheet 2, E2. Divide it by 12 because $D$ is in feet. Excel will enter the result of this calculation in Cell #B2.

In the same way enter the solids acceleration formula, $W \cdot V_f^2/4640$, in Cell #C2. For $W$, enter #C3 and for $V_f$, enter #B10 from worksheet 1. Excel will enter the result in Cell #C2.

Now enter the formula for flow of solids, $\Delta P_g \cdot K \cdot R$, in Cell #D2. For $K$ and $R$, enter Cell #B14 and Cell #B15 from worksheet 1, respectively. Result will be entered in Cell #D2 in worksheet 3.

Now enter the formula for the elevation of gas, $(\Delta Z \cdot \rho_g \cdot g)/(144 \cdot V_f \cdot g_c)$, in Cell #E2. Because this pipe section is horizontal as shown in worksheet #2, this pressure drop will be zero.

Similarly, enter the formula for the elevation of solids, $(\Delta Z \cdot W \cdot g)/(144 \cdot V_f \cdot g_c)$, in Cell #F2. Because this pipe section is horizontal as shown in worksheet #2, this pressure drop will also be zero.

Miscellaneous pressure drop in Cell #G4 will also be zero in this section.

Now add all of the pressure drops in Cell #H2 by using the formula $(= \Sigma(B2,C2,D2,E2,F2,G2))$.
3.4.2 Gas Density, Gas Pressure, and Gas Velocity Calculations

First section’s outlet gas pressure in Cell #M2 is the difference between the inlet pressure and the pressure drop in this section. In Cell #M2 use the formula, \( P_{out} = P_{in} - \sum_{i=2}^{n} (L_i - H_i) \).

Outlet gas density is calculated in Cell #K2 by using the formula:

\[ \rho_g = \frac{28 \cdot P_{out}}{19.32 \cdot (T_{out} + 273)} \]

Outlet gas velocity in Cell O2 is calculated by using the formula:

\[ V_g = \frac{V_{in} \cdot \rho_{in}}{\rho_g} \]

3.4.3 Calculations for Pipeline Sections 2 to 20

Method for calculations for these sections is the same as for section 1, except that the outlet conditions for the preceding section become the inlet conditions for the next section.

3.5 Step 5

Total pressure drop in the conveying system is totaled by adding the pressure drops in Cells H2 to H21. As shown in worksheet 3, this pressure drop comes to 7.58 psi. The vacuum blower should be able to handle this pressure. If not, run another calculation using a 6 inch pipeline and by entering 6 in cells E2 to E21 in worksheet 2. No other changes in the input data or the formulae are needed. Compare both of the results and if the pressure drop in the 6 inch line is too low, use a stepped pipe line starting from 4 inch and increasing to 6 inch about midway in the conveying line.

4. Conclusion

For most process and operating engineers the pressure drop calculation method described in this article should be easy to use, to understand, and to study the effect of different variables on system design. It requires only an understanding of Excel and a basic understanding of pneumatic conveying. This article does not give formulae for the calculation of conveying velocity because this subject has already been covered in various published articles.

References


Research papers published by Dr. F. A. Zenz in the 70’s and 80’s.

Particle Science Research Institute (PSRI) Reports published by Dr. Zenz.

 Appendix 1

WORKSHEET NO. 1: CONVEYING SYSTEM INPUT DATA

<table>
<thead>
<tr>
<th>Cell Numbers</th>
<th>A</th>
<th>B</th>
<th>C</th>
<th>D</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>Type of conveying system</td>
<td>Vacuum type</td>
<td></td>
<td></td>
</tr>
<tr>
<td>2</td>
<td>Material to be conveyed</td>
<td>Polyethylene pellets</td>
<td></td>
<td></td>
</tr>
<tr>
<td>3</td>
<td>Solids Conveying Rate</td>
<td>10,000 lbs/hr</td>
<td>W</td>
<td></td>
</tr>
<tr>
<td>4</td>
<td>Pipeline Material</td>
<td>Aluminum, Schedule 10 pipe, internally scored</td>
<td>L</td>
<td></td>
</tr>
<tr>
<td>5</td>
<td>Conveying Line Configuration</td>
<td>See Worksheet 2</td>
<td></td>
<td></td>
</tr>
<tr>
<td>6</td>
<td>Pipe Inside Diameter</td>
<td>4 inch (d) or 0.333 ft (D)</td>
<td>D</td>
<td></td>
</tr>
<tr>
<td>7</td>
<td>Gas used for conveying</td>
<td>Ambient Air at 25 C and 14.7 psia</td>
<td></td>
<td></td>
</tr>
<tr>
<td>8</td>
<td>Gas Inlet Temperature</td>
<td>25 C</td>
<td>t</td>
<td></td>
</tr>
<tr>
<td>9</td>
<td>Inlet Gas Density</td>
<td>0.075 lbs/cu ft</td>
<td>( \rho_g )</td>
<td></td>
</tr>
<tr>
<td>10</td>
<td>Gas velocity at inlet of conveying system</td>
<td>65 ft/sec</td>
<td>Vg</td>
<td>Based on Test Data</td>
</tr>
<tr>
<td>11</td>
<td>Solids Velocity</td>
<td>0.8 x Vg</td>
<td>Vp</td>
<td>Based on Test Data</td>
</tr>
<tr>
<td>12</td>
<td>Gas mass flow rate</td>
<td>Hand calculate based on pipe diameter, gas density, and gas velocity (all at inlet conditions) = 1528 lbs/hr</td>
<td></td>
<td></td>
</tr>
<tr>
<td>13</td>
<td>Solids to Gas mass flow Ratio, R</td>
<td>Hand calculate based on solids conveying rate and gas mass flow rate, lbs/hr ( (= \frac{B3}{B12}) = 6.54 )</td>
<td>R</td>
<td></td>
</tr>
<tr>
<td>14</td>
<td>Solids Friction Factor (K)</td>
<td>1.2</td>
<td>K</td>
<td>Based on Test Data</td>
</tr>
<tr>
<td>15</td>
<td>Pipe line Roughness Factor</td>
<td>0.0005</td>
<td></td>
<td>Based on Test Data</td>
</tr>
<tr>
<td>16</td>
<td>Fanning Friction Factor</td>
<td>Use Excel to calculate based on solids friction factor K, pipe diameter D, and Reynolds Number, using Equation 7 in the formula bar = 0.00592</td>
<td>f</td>
<td></td>
</tr>
</tbody>
</table>
### Appendix 2

**WORKSHEET NO. 2: PIPE LINE SECTIONS DATA**

<table>
<thead>
<tr>
<th>Section Number</th>
<th>Pipe line component</th>
<th>Orientation</th>
<th>Inside Diameter (d), inches</th>
<th>Section Equivalent Length (L), feet</th>
<th>Cumulative Equivalent Length, feet</th>
</tr>
</thead>
<tbody>
<tr>
<td>2</td>
<td>pipe</td>
<td>Horizontal</td>
<td>10</td>
<td>4</td>
<td>10</td>
</tr>
<tr>
<td>3</td>
<td>pipe</td>
<td>Horizontal</td>
<td>10</td>
<td>4</td>
<td>20</td>
</tr>
<tr>
<td>4</td>
<td>pipe</td>
<td>Horizontal</td>
<td>10</td>
<td>4</td>
<td>30</td>
</tr>
<tr>
<td>5</td>
<td>pipe</td>
<td>Horizontal</td>
<td>10</td>
<td>4</td>
<td>40</td>
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<tr>
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<td>4</td>
<td>50</td>
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<td>4</td>
<td>60</td>
</tr>
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<td>pipe</td>
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<td>10</td>
<td>4</td>
<td>70</td>
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<tr>
<td>9</td>
<td>pipe</td>
<td>Horizontal</td>
<td>10</td>
<td>4</td>
<td>80</td>
</tr>
<tr>
<td>10</td>
<td>90° Bend vertical</td>
<td>Horizontal</td>
<td>4</td>
<td>20</td>
<td>100</td>
</tr>
<tr>
<td>11</td>
<td>pipe</td>
<td>Vertical</td>
<td>10</td>
<td>4</td>
<td>170</td>
</tr>
<tr>
<td>12</td>
<td>pipe</td>
<td>Vertical</td>
<td>10</td>
<td>4</td>
<td>180</td>
</tr>
<tr>
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### Appendix 3

**WORKSHEET NO. 3: PRESSURE DROP CALCULATIONS**

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<th>Outlet Gas Density</th>
<th>Inlet Pressure</th>
<th>Outlet Pressure</th>
<th>Inlet Gas Velocity</th>
<th>Outlet Gas Velocity</th>
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Total Pressure Drop: 7,550

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